

The comparison of radial and axial flow porous burners from viewpoint of output radiative heat transfer and emissions

N. Ghiasi Tabari*, M.R. Astaraki and A.H. Arabi

Islamic Azad University-Dashtestan branch, Dashtestan, Bushehr, Iran

(Received June 22, 2012, Revised September 8, 2012, Accepted September 11, 2012)

Abstract. In this paper, two types of porous burners with radial and axial flow have been modeled numerically and compared. For this purpose, governing equations were solved one-dimensionally for methane-air premix gas. The mechanism used in simulating combustion phenomenon was 15 stage reduced mechanism based on GRI3.0. In order to compare the two burners, the inlet flow rate and fuel-air ratio have been assumed equal for the two burners. The results of the study indicated that reduction in speed and increase in cross-section area in the direction of flow have a considerable influence on the behavior of radial burner in comparison to axial burner. Regarding temperature distribution inside the burner, it was observed that the two above mentioned factors can be influential in temperature of flame propagation region. Also, regarding distribution of CO and NO emission, the results indicate that the porous radial burner has lower emissions in comparison to the axial once. The output radiative heat transfer efficiency of the two burners was also compared and in this case also even the radial porous burner was found to be preferable.

Keywords: radial porous burner; axial porous burner; emissions; speed reduction

1. Introduction

One of the possible configurations for porous burners is cylindrical configuration. In this configuration, two types of flows can be assumed, one is a flow which moves in the burner axially. This type of flow was investigated by Khosravy *et al.* (2008). in cylindrical geometry and the effect of pressure drop was studied on performance of burner. In another study, they also investigated the effect of lateral heat conduction in cylindrical geometry with axial flow Khosravy (2007).

Since combustion causes a sudden increase in temperature, as a result density decreases, therefore because of continuity the speed of gases increases suddenly, which leads to instability in flame formation. In porous burners, increasing the cross-section of the burner after flame zone is one of the proposed solutions, but increase in cross section causes dispersions in the movement pattern of the flow and the control of which is sometimes difficult. porous burners with radial flow is able to overcome this problem, because combustion inside porous medium with radial flow causes to a decrease in speed by increase in radius. Khosravy and Mohamad (2006) suggested this type of flow

* Corresponding author, Dr, E-mail: Ghiasi@diau.ac.ir

for improvement of flame stabilization and better heat recycling in burners. In addition to radial flow in cylindrical geometry and radial flow in spherical geometry is also presented with regards to improvement in flame stabilization Susie and Andrew (2008).

In other words, for high inlet speeds for which a stable flame cannot be achieved in axial burners, in radial burner a stable flame can be formed. These kinds of burners have other advantages too, like reduction in CO emission. the major reason of which is the decrease of speed in the direction of radius and as a result an increase in residence time. Also one of the geometric advantages of such a system is the small and compact size of the burner in comparison to a burner with axial flow.

Several numerical solutions have been proposed for porous burner with radial flow. Zhdanok *et al.* (1998) studied flame stability in cylindrical and spherical porous burners and compared flame stability in cylinder and sphere. They proposed an analytical solution for the problem with one-temperature assumption, in fact they assumed that the volumetric internal heat transfer coefficient is infinite. Also, they solved the problem with two-temperature model and using Arrhenius form for modeling combustion numerically. In their analytical solution, for some values of inlet flow rate two radii were obtained for stabilization point, in a way that if ignition happens between these two points, the flame forming region tends toward the shorter radius. They also found that in spherical coordinate in order to have a stable flame inside porous area, a longer length should be preheated in comparison to that in cylinder. In another paper Zhdanok *et al.* (2000) analyzed the effect of medium transparency on the performance of cylindrical and spherical porous burner. The results of the study showed that output radiation efficiency is more for transparent material. They also studied the effect of transparency of medium on maximum temperature of porous medium and found out that the maximum temperature for a transparent material is 50 to 150 Kelvin less. In both numerical solutions mentioned above, single-step chemical kinetics was used for simulation of combustion and just the stability of the flame was dealt with and nothing was discussed about the effect of this radial flow on emissions.

Kamal and Mohamad (2006) performed an experimental study on porous burner with radial flow. In their study, they reported temperature distribution, emissions, and output radiative heat transfer efficiency and also investigated the effect of swirl of flow on burner performance. Their experimental study results indicated that because of decrease in speed in the direction of flow and more radiative heat transfer in porous medium, the radial flow in porous burner can also cause a decrease in emissions.

In the present paper two porous burners, one with axial flow and the other with radial flow have been simulated numerically and have been compared from various viewpoint like speed, temperature, emissions and output radiative heat transfer efficiency. In order to study the governing equations have been solved one-dimensionally, One-dimensional assumption has acceptable precision to predict the behavior of an actual porous burner whit isolated lateral walls Khosravy *et al.* (2007). Also comparison has been performed by taking into account equal fuel flow rate and fuel-air ratio for two porous burners.

2. The governing equations and solution method

The governing equations generally include continuity, gas and solid energy, radiative transfer equation¹, gas species and gas state equation.

$$\frac{d}{dx}(\rho u A \phi) = 0 \quad \text{continuity (1)}$$

$$\rho u A \phi \frac{dT_g}{dx} - \frac{1}{c_{pg}} \frac{d}{dx} \lambda_s A \phi \frac{dT_g}{dx} + \frac{A}{c_{pg}} \phi \sum_{k=1}^K \rho Y_k V_k c_{pk} \frac{dT_g}{dx} \quad \text{gas energy (2)}$$

$$+ \frac{A}{c_{pg}} \phi \sum_{k=1}^K \omega_k h_k W_k - A \phi H_V (T_s - T_g) = 0$$

$$\frac{1}{c_{ps}} \frac{d}{dx} \lambda_s A_s \frac{dT_g}{dx} - A_s H_V (T_s - T_g) - \frac{d(A_s q_{rad})}{dx} = 0 \quad \text{Solid energy (3)}$$

$$\frac{dI(\vec{r}, \hat{s})}{ds} = -\beta I(\vec{r}, \hat{s}) + \sigma_a I_b + \frac{\sigma_s}{4\pi} \int_{4\pi} I(\vec{r}, \hat{s}') \Phi(\hat{s}', \hat{s}) d\Omega' \quad \text{Radiative transfer (4)}$$

$$\rho u A \phi \frac{dY_k}{dx} + \frac{d}{dx} (\rho A \phi Y_k V_k) - A \phi \omega_k W_k = 0, \quad (k = 1, \dots, K) \quad \text{Gas species (5)}$$

$$\rho = \frac{p \bar{W}}{RT} \quad \text{gas state (6)}$$

In Eq 3, term q_{rad} is the radiative heat flow, which is calculated from equation

$$\frac{dq_{rad}}{dx} = \sigma_a (4\sigma T^4 - G), \quad G = \int_{4\pi} I d\Omega \quad (7)$$

In the equations above, when the burner has axial flow, the cross section of flow (A) is constant, and when the burner has radial flow, the cross section of flow is variant and is equal to $A = 2\pi x$.

In order to solve the equations above, the famous PREMIX code from CHEMKIN group which was originally used for simulating one-dimensional free and laminar flame Kee *et al.* (1985) was developed for simulating combustion inside porous media. For this purpose solid Energy and radiative transfer equations were added to the set of the above mentioned solvable equations by PREMIX cod. also some changes were made in PREMIX gas energy equation in order to solve combustion in porous media in PREMIX code. Solving the equations is done in three stages:

First, a chemical species distribution is found by using a temperature preliminary guess. In the second stage, by using distribution obtained from first stage as preliminary guess, energy, species, and continuity equations are solved without taking into account the radiation and in the last stage, all equations are solved implicitly by using the previous stage results as preliminary guess.

In order to solve radiative transfer equation, the Discrete Ordinates Method² was used. In this method, radiative heat transfer equation is transformed into a partial differential equations set, in which each equation is written for one space direction. The summation of these directions should cover a sphere with 4π space degrees.

According to studies done on combustion mechanisms, a suitable chemical kinetic was chosen which was suitable from viewpoint of calculations time and precision of results Sung *et al.* (2001). Khosravy *et al.* (2008) investigated Precision of GRI3.0 and Miller reduced mechanism in comparison to full mechanism, their study was displayed satisfactory agreement between 15 stage

¹RTE

Table 1. boundary conditions

RTE	species	Solid energy	Gas energy	continuity
$I(\vec{r}, \hat{s}) = \varepsilon_{in} I_b + \frac{1 - \varepsilon_{in}}{4\pi} \times \int_{4\pi} I(\vec{r}, \hat{s}') \cdot \hat{s}' \cdot \hat{n} d\Omega'$	$Y = Y_{in}$	$H_V(T_{g, in} - T_s) + \sigma \varepsilon (T_{sur}^4 - T_g^4) = -k_s \frac{dT_s}{dx}$	$\dot{m} c_{pg} (T_{g, in} - T_s) = -k_g \frac{dT_g}{dx}$	$u = u_{in}$ inlet
$I(\vec{r}, \hat{s}) = \varepsilon_{out} I_b + \frac{1 - \varepsilon_{out}}{4\pi} \times \int_{4\pi} I(\vec{r}, \hat{s}') \cdot \hat{s}' \cdot \hat{n} d\Omega'$	$\frac{dY}{dx} = 0$	$H_V(T_{g, out} - T_s) + \sigma \varepsilon (T_{sur}^4 - T_g^4) = -k_s \frac{dT_s}{dx}$	$\frac{dT_g}{dx} = 0$	- outlet

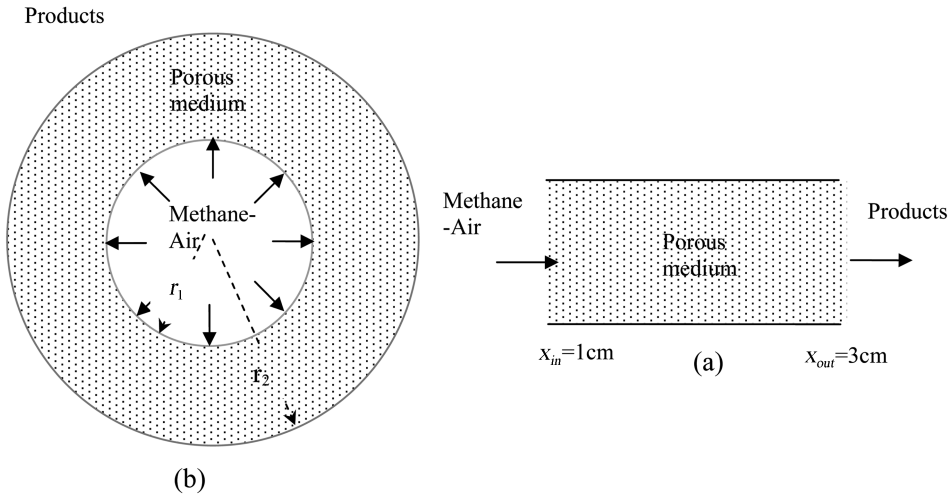


Fig. 1 schematic figure of two axial and radial flow porous burners

reduced mechanism based on GIR3.0 in comparison to GRI3.0 mechanism. In this study The mechanism used in simulation are 15 stage reduced mechanism based on GRI3.0.

Boundary conditions of Eqs. (1)-(6) is shown in Table 1.

3. The geometry of radial and axial porous burners

A schematic picture of two axial(a) and radial(b) flow porous burners has been showed in Fig. 1. The burner which was experimented in Kamal and Mohamad (2006) study had external and internal radii of 3 and 1 centimeters and the same values were kept in this study for modeling. The thickness of axial burner is also 2 centimeters like the radial burner. The material property used in modeling of both burners are displayed in Table 2.

Table 2. Material property used in modeling of both burners (Zhou and Pereira 1997, Amanda and Janet 2004)

$\beta = 1707m^{-1}$	$\sigma_s = 1365m^{-1}$
$H_V = 2.5 \times 10^7 W/m^3 \cdot K$	$\lambda_s = 3.6 W/m \cdot K$
$\rho_s = 510 kg/m^3$	$\phi = 0.87$
$c_{ps} = 824 J/kg \cdot K$	$\varepsilon = 0.3$

4. Results and discussion

In order to compare two axial and radial porous burners, the flow rate of inlet and fuel-air ratio has been assumed as equal for both burners, therefore both burners have equal powers. The cross section of flow in inlet of the radial burner is equal to cross section of flow in axial burner. The parameters dealt with in this section are burner output radiative heat transfer efficiency, amount of emissions, and speed and temperature profile.

5. Temperature profile

In Fig. 2 the temperature profile of two burners being under study and Kamal and Mohamad (2006) experimental study results are displayed. It can be observed in the figure that the temperature of gas in axial flow burner is more than burner with radial flow. The reason for this can be ascribed to the difference between radiative heat transfer in two burners. Since in radial burner the cross section area increases in the direction of the flow, the radiative heat transfer is more than that in the case of axial flow. As a result, more heat is transferred by radiation to preheat section and the area out of flame propagation region, and this causes temperature decrease in flame propagation region in radial porous burner in comparison to axial porous burner. On the other hand, radiative heat transfer field is more homogeneous in radial mode. According to the reasons mentioned above, it is expected that the gas temperature for a burner with radial flow in flame propagation region would be low and in preheat section be higher than axial flow burner. Temperature distribution in flame propagation region is displayed in Fig. 3. The temperature of radial burner at the beginning of flame forming region is about 50 °K more than axial burner, which reaches zero near flame propagation

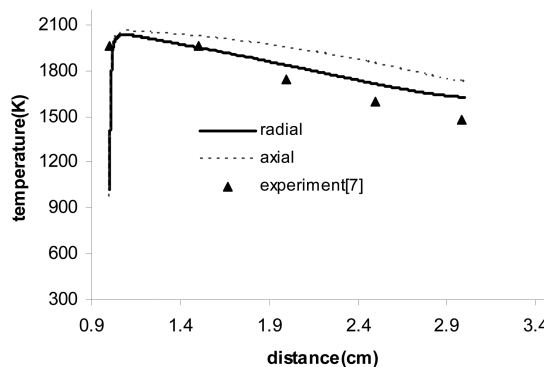


Fig. 2 temperature distribution of both burner versus distance

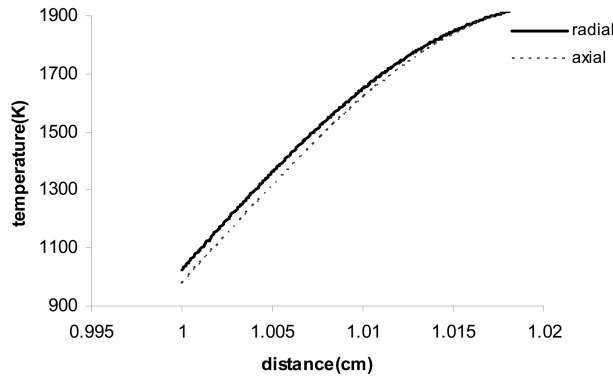


Fig. 3 temperature distribution of both burner in flame propagation zone versus distance

region, then the temperature of axial burner is increased to a point that it reaches 100 °K more than radial burner at outlet.

6. Speed profile

In Fig. 4 the graph of speed distribution in terms of burner length for two radial and axial porous burners has been displayed.

In radial burner the speed in direction of the flow is lower in comparison to axial porous burner for two reasons:

The first reason is the increase in cross section area in the direction of flow, which causes to decrease in speed because of continuity. The second reason is the lower gas temperature, which is followed with higher density. Due to continuity The higher density causes to speed reduction.

7. Emissions

In general, in a porous burner emissions are lower in comparison to burner with free flame for a specific burner power and this is an important reason for using porous burners. According to studies

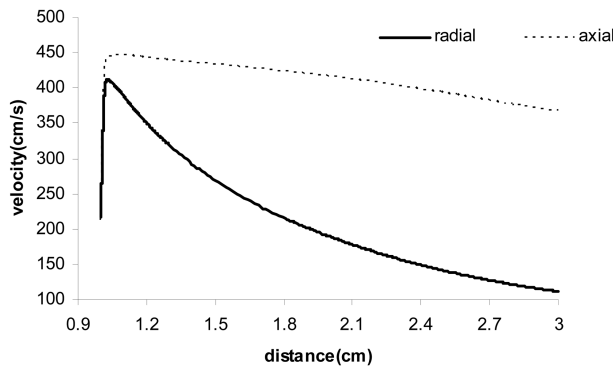


Fig. 4 speed distribution in axial and radial burner versus distance

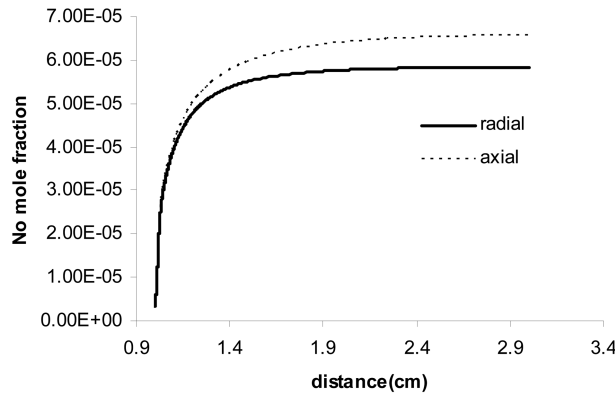


Fig. 5 NO mole fraction profile

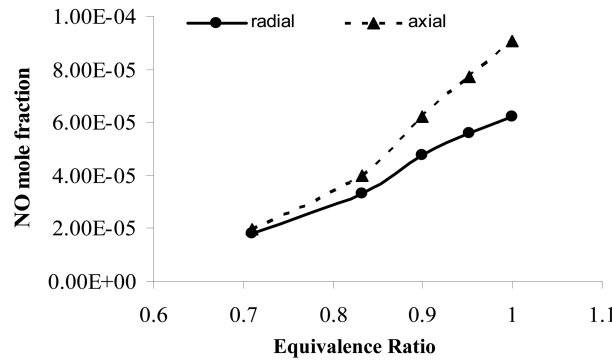


Fig. 6 NO mole fraction versus equivalence ratio

done, the maximum temperature of the flame is the most influential factor in NO production rate Turns (2000). Since the maximum temperature of the flame in radial burner is lower than that in axial burner, it is expected that a lower amount of NO is produced. In Fig. 5 mole fraction graph of NO pollutant has been displayed in terms of the distance inside axial and radial burners.

The reason for the difference between amount of NO emission in two burners can be justified by two reasons: first, As was mentioned, the temperature of flame propagation region in radial porous burner is lower than axial porous burner because of higher radiative heat transfer and this factor causes to decrease in NO emissions in radial burner. second, decrease in speed in radial burner and as a result increase in residence time causes to increase in NO emission Kamal and Mohammad (2006), but Fig. 6 shows that the first reason is more effective. This figure displays NO emission versus equivalence ratio in constant Firing Rate. The value of Firing Rate is stated as Eq. (8)

$$FR = \dot{m}_{fuel} \cdot LHV \tag{8}$$

In Eq. (8), \dot{m}_f and LHV are inlet fuel flow rate and lower heat value of fuel, respectively. It can also be observed in Fig. 6 that with increase in equivalence ratio, the difference in NO emission between radial and axial burner increases.

In radial porous burner, 31% decrease in NO emission is observed in comparison to axial porous

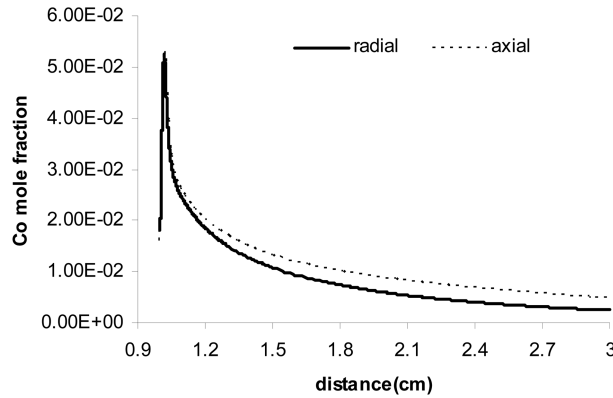


Fig. 7 CO mole fraction profile in radial and axial porous burners

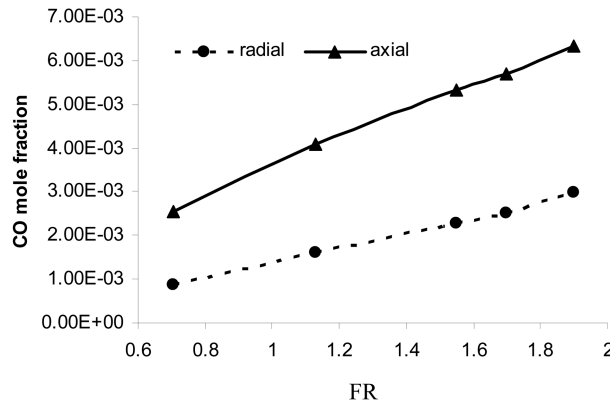


Fig. 8 CO mole fraction versus equivalence ratio

burner in stoichiometric mixture, but about CO pollutant the decrease is more. In Fig. 7, CO mole fraction versus distance is displayed.

According to the Fig. 7, at the beginning of flame formation region the amount of CO increases with a high gradient and reaches approximately equal in two burners. Then the amount of CO decreases from that point to the end of both burners, but it decreases with higher intensity in radial burner in comparison to axial burner. The reason for this is related to the speed reduction in the direction of the radius in radial burner. decrease in speed causes an increase in residence time and therefore more CO is transform into CO₂. in a way that the outlet CO of the radial burner is 2290 ppm, but this amount in an axial burner is 5541 ppm, It means that, in radial porous burner CO emission is about 58% lower than that in axial porous burner.

It has to be mentioned that the amount of CO production in experimental study Kamal and Mohammad (2006) for stoichiometric mixture was 2100 ppm. Since the present modeling is one dimensional, therefore the results obtained in this study have satisfactory agreement with experimental results.

Fig. 8 displays CO mole fraction for radial and axial porous burner in terms of FR in stoichiometric fuel-air ratio. In Fig. 8 the parameter which has stayed constant is the ratio of fuel-air mixture, that means that by keeping the mixture ratio the inlet speed has increased. Fig. 8 shows

that in both burners by increase in FR, the amount of produced CO increases, but the intensity of the increase in radial burner is lower in comparison to axial burner. In general, by an increase in FR, since the inlet speed increases and residence time decreases, more CO is produced.

8. Output radiative heat transfer efficiency

One of the other parameters dealt with in this study is the radiative output efficiency, which is defined as Eq. (9).

$$\eta_{rad} = \frac{\sigma \varepsilon A_{out} (T_s^4 - T_{sur}^4)}{FR} \tag{9}$$

The results of the study indicate that the temperature of porous burner with radial flow is lower than axial flow in both gas and solid phases. In a way that for example in stoichiometric fuel-air ratio, the temperature of solid at outlet of radial burner is 1542 and in axial burner is 1768 K and at first look it seems that the axial burner has more radiative heat transfer to outside environment, but in fact the radiative heat transfer to outside of burner in radial burner is more due to larger heat transfer area. In a way that this value in radial burner is 367 KW and in axial burner 211 KW, while the amount of FR for both burners is 1550 KW, therefore output radiative heat transfer efficiency in

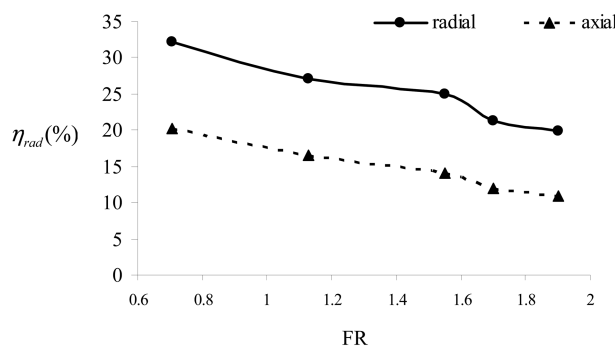


Fig. 9 output radiative heat transfer efficiency versus FR

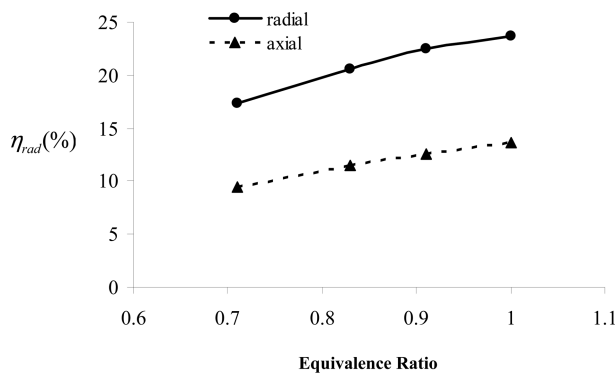


Fig. 10 output radiative heat transfer efficiency versus equivalence ratio

radial burner will be 23.7% and in axial burner 13.6%. Fig. 9 displays radiative output efficiency in terms of FR for stoichiometric mixture ratio. By an increase in FR the temperature increases at outlet of the burner and as a result radiative heat transfer to outside environment increases, but it is obvious in the Fig. 9 that by increase in FR, since the denominator of the fraction of Eq. (8) increases, output radiative heat transfer efficiency decreases. Bara and Ellzey also found a similar process about axial flow burner Amanda and Janet (2004).

In Fig. 10 output radiative heat transfer efficiency shows for a constant FR value in terms of equivalence ratio. Figs. 9 and 10 indicates that radiative output efficiency of radial porous burner is more than axial porous burner.

9. Conclusions

In this study, two radial and axial porous burners have been compared from viewpoint of speed and temperature distribution, emissions and output radiative heat transfer efficiency. A burner with radial flow has positive influences on mentioned parameters. The most important characteristics which cause to preference of radial porous burner in comparison to axial porous burner are increase in radiative heat transfer and decrease in emission of pollutants like NO and CO.

The results from numerical solution indicate that since cross section area increases in the direction of the flow, the transferred heat by radiative from flame propagation region increases and this causes reduction in the temperature of flame propagation region, as a result NO emission decreases. On the other hand, the decrease in speed in the direction of radius causes to reduction in CO and NO emission, that the reason for this is increase in residence time. More heat transfer area is another preference of radial porous burner in comparison to axial ones that causes to improvement output radiative heat transfer efficiency. Moreover, the results indicate that the maximum efficiency occurs in a constant heat power at stoichiometric mixture.

References

- Amanda, J.B. and Janet, L.E. (2004), "Heat recirculation and heat transfer in porous burners", *Combust. Flame*, **137**(1-2), 230-241.
- Kamal, M.M., and Mohamad, A.A. (2006), "Combustion in porous media", *Proceedings of the Institution of Mechanical Engineers*, Aug.
- Kamal, M.M. and Mohamad, A.A. (2006), "Development of cylindrical porous-medium burner", *J. Porous Media*, **9**, 469-481.
- Kee, R., Grcar, J., Smooke, M. and Miller, J. (1985), *A FORTRAN program for modeling steady laminar one dimensional premixed flames*, Technical Report SAND85-8240, Sandia National Laboratories.
- Khosravi El-Hossaini, M. (2007), *Modeling and numerical analysis of cylindrical porous radiant burner*, Iran, Tehran, Tarbiat Modares University, PhD theses.
- Khosravy EL-Hossaini, M., Maerefat, M. and Mazaheri, K. (2008), "Numerical investigation on the effects of pressure drop on thermal behavior of porous burner", *J. Heat Trans.-T. ASME*, **130**, 032601-1.
- Khosravy EL-Hossaini, M., Maerefat, M. and Mazaheri, K. (2008), "Numerical modeling of porous radiant burner using full and reduced kinetics mechanism", *Iran. J. Chem. Chem. Eng.*, **27**(1).
- Sung, C.J., Law, C.K. and Chen, J.Y. (2001), "Augmented reduced mechanisms for NO emission in methane oxidation", *Combust. Flame*, **125**(1-2), 906-919.
- Susie, W. and Andrew, T H. (2008), "Porous burners for lean-burn applications", *Prog. Energ. Combust.*, **34**(5),

667-684.

Turns, S.R. (2000), *An introduction to combustion: concept and application*, 2nd Ed., McGraw-Hill.
 Zhdanok, S.A., Dobrego, K.V. and Futko, S.I. (1998), "Flame localization inside axis-symmetric cylindrical and spherical porous media burners", *Int. J. Heat Mass Tran.*, **41**(22), 3647-3655.
 Zhdanok, S.A., Dobrego, K.V. and Futko, S.I. (2000), "Effect of porous media transparency on spherical and cylindrical filtration combustion heater performance", *Int. J. Heat Mass Tran.*, **43**(18), 3469-3480.
 Zhou, X.Y. and Pereira, J.C.F. (1997), "Numerical study of combustion and pollutant formation in inert nonhomogeneous porous media", *Combust. Sci. Technol.*, **130**(1-6), 335-364.

Nomenclature		Greek symbols	
A	Cross-section area	λ	Heat conductivity
C_p	Heat capacity at constant pressure	σ_a	Absorption factor
H_v	Volumetric heat transfer between gas and solid phases	σ_s	Scattering albedo
I	Radiation intensity	β	Extinction coefficient
\dot{m}	Flow rate	ε	Emissivity
P	Pressure	Ω	Space angle
q_{rad}	Radiative heat flux	ϕ	porosity
R	Gas constant	φ	Equivalence ratio
r	Radial direction	Φ	Phase function
\hat{s}	Space direction	$\dot{\omega}$	Production rate
T	Temperature		
Nomenclature		subscripts	
u	Velocity	s	Solid
V	Diffusion velocity	k	Species counter
W	Molecular weight	in	inlet
x	Axial coordinate	out	outlet
Y	Mass fraction	Sur	Surround
		g	gas